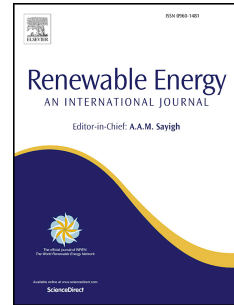


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# An All-day Cooling System that Combines Solar Absorption Chiller and Radiative Cooling

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**Abstract:** Although the solar-powered absorption chiller is recently a trending technology for space cooling of buildings, it requires a bulky thermal storage device and complex installations to achieve all-day cooling. In this paper, a new system that couples the solar-driven absorption chiller and radiative sky cooling is proposed to realize 24-h continuous cooling with less floor space and smaller thermal storage. This system involves a specialized module that utilizes the medium temperature flat panel solar collector on its top layer and a selective radiative cooling absorption layer on the bottom layer; The top layer faces the sky during the daytime to collect solar thermal energy to drive the absorption chiller, and it will be flipped to the bottom layer at nighttime to realize radiative cooling. The proposed system is analyzed by coupling the steady-state models of each subsystem and a cooling load model, which are later applied to evaluate the cooling performance under varying weather conditions within a day. The simulation results show that the system can stably meet the cooling demand of 70 m<sup>2</sup> room while only needing half the floor area and a thermal storage tank that is 4 times smaller than the traditional PT-AC system.

**Keywords:** Solar Absorption Chiller; Radiative Cooling; All-day Cooling; Selective Absorption Coatings

**Nomenclature:**

## *Abbreviations*

COP – Coefficient of Performance

PT – Photothermal

RSC – Radiative Sky Cooling

AC – Absorption chiller

ARP – Alternating period of refrigeration

FPSC – Flat plate solar collector

## *Variables*

$A$  – Area (m<sup>2</sup>)

$Q$  – Heat (W)

# An All-day Cooling System that Combines Solar Absorption Chiller and Radiative Cooling

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FPSC – Flat plate solar collector

**Variables**

$A$  – Area (m<sup>2</sup>)

$Q$  – Heat (W)

- 42  $U$  – Heat loss coefficient ( $W/(m^2 \cdot K)$ )  
 43  $F'$  – Collector's efficiency factor  
 44  $F_R$  – Collector's heat removal factor  
 45  $I$  – Solar radiation ( $W/(m^2)$ )  
 46  $V$  – Velocity (m/s)  
 47  $h$  – Heat transfer coefficient ( $W/(m^2 \cdot K)$ )  
 48  $T$  – Temperature (K)  
 49  $k$  – Thermal conductivity of air ( $W/(m \cdot K)$ )

50

51 ***Greek symbols***

52

- 53  $\eta$  – Efficiency  
 54  $\varepsilon$  – Radiative emissivity  
 55  $\lambda$  – Wavelength (nm)  
 56  $\tau$  – Transmittance  
 57  $\alpha$  – Absorptivity

58

59 ***Subscripts***

60

- 61  $amb$  – Ambient  
 62  $bot$  – Bottom  
 63  $sky$  – Sky  
 64  $ave$  – Average  
 65  $f$  – Fluid  
 66  $i$  – Inlet  
 67  $o$  – Outlet  
 68  $s$  – Solar energy  
 69  $m$  – Mean  
 70  $top$  – Top  
 71  $side$  – Side  
 72  $L$  – Loss  
 73  $Load$  – Load  
 74  $E$  – Evaporator  
 75  $G$  – Generator  
 76  $b$  – Black body

77

78 ***Constants:***

79

- 80  $\sigma = 5.67 \times 10^{-8} \text{ W}/(m^2K)$  – Stefan Boltzman constant

81 **1.INTRODUCTION**

82 The demand for energy by humanity has increased dramatically with population growth  
 83 and the development of science and technology. However, this has worsened

84 environmental problems such as the intensifying greenhouse effect due to increased  
85 fossil fuel consumption. In particular, building cooling (including services and  
86 households) occupies a very significant part of the total energy demand [1], which may  
87 be up to 40% globally or 37% in China [2]. Therefore, the use of renewable energy,  
88 such as solar energy [3, 4], for building cooling and temperature regulation has become  
89 an increasingly important practice, so governments of various countries are currently  
90 promoting research on solar energy utilization [5, 6].

91  
92 Currently, the heat pump is the most widely used method of refrigeration, but they do  
93 have various disadvantages. For example, despite being very widely used in air  
94 conditioners, the vapor compression cycle (VCC) involves refrigerants that can  
95 significantly damage the natural environment when leaked into it. The thermoelectric  
96 cooler (TEC) has a simpler structure and does not require moving mechanical parts, but  
97 its cooling performance is insufficient for buildings [7]. Hence, the absorption chiller  
98 (AC) is another emerging cooling technology. Despite having a relatively low cooling  
99 performance over the VCC, the AC can utilize lower grade heat to produce cooling  
100 energy, so it can be easily coupled to a solar collector or a certain facility that produces  
101 significant heat [8]. Meanwhile, passive cooling methods such as radiative sky cooling  
102 (RSC) have also been favored by many researchers because they do not require any  
103 energy consumption [9-11], but their specific cooling capacities are too low for  
104 economical use. Overall, optimizing the AC and RSC in terms of their designs and  
105 method of operation is an essential step for drawing these technologies closer to  
106 widespread commercial use.

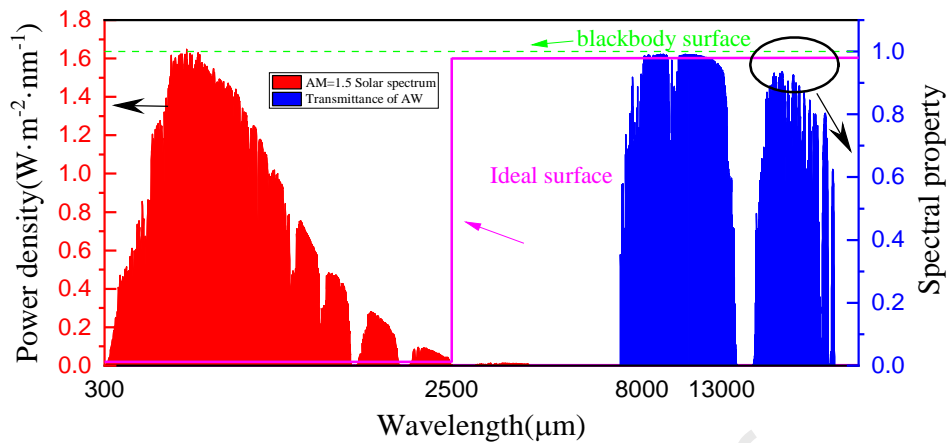
107  
108 One important aspect of solar-driven absorption chillers is the appropriate working  
109 solution within the thermodynamic system. A comparative study of different possible  
110 solutions was conducted by Kim et al. [12], who found that the total cost of a single-  
111 effect LiBr-H<sub>2</sub>O absorption system was the lowest. This finding is consistent with that  
112 by Ahmed et al. [13] who evaluated the performance of an integrated cooling plant  
113 having both a free cooling system and solar-powered single-effect LiBr-H<sub>2</sub>O based AC.  
114 Alternatively, other researchers also considered trying to apply a higher temperature  
115 solar heat collector as the heat source, which would generally require the use of multi-  
116 effect ACs. Specifically, Xu et al. [14] compared different Compound Parabolic  
117 Concentrator based solar absorption cooling systems with single, double, and multiple  
118 effect absorption chillers. Although this study proved that the double effect AC can  
119 allow a higher input temperature and hence yield higher COPs, the system complexity  
120 significantly increases, and the increased temperature difference relative to the ambient  
121 may cause slower dynamic responses. Actually, the single effect AC is proven to still  
122 be an acceptable choice by Azhar et al. [15] even under the harsh hot and humid climatic  
123 conditions of New Delhi. Hence, this paper will maintain the use of single effect ACs.

124  
125 Besides solar energy, another cooling energy source in the sky is using the deep outer  
126 space as a heat sink, which is achieved by radiative sky cooling (RSC) [10, 11, 16].  
127 Notably, RSC is a critical heat flow component in the Earth's heat budget system as a

128 means to remove the incoming solar irradiation energy and balance the earth's surface  
129 temperature to habitable levels [10]. In regards, a specific RSC module aims to adopt a  
130 material with minimized solar irradiation absorption and maximized emissivity in the  
131 infrared band so that an environment with a temperature lower than ambient can be  
132 generated. To realize the above aims, the appropriate selective absorption coatings  
133 choice is critical. As Figure 1 shows, the selective absorbing coatings have high  
134 emissivity in the “atmospheric window” band ( $8\ \mu\text{m}$  to  $13\ \mu\text{m}$ ) so that infrared  
135 energy can radiate into the outer space efficiently. In a recent study of the RSC, an  
136 example material is an integrated photonic solar reflector and thermal emitter as  
137 introduced by Raman et al. [17], which could reflect 97 percent of incident sunlight  
138 while emitting strongly and selectively in the  $8\ \mu\text{m}$  to  $13\ \mu\text{m}$  window. As a result,  
139 the cooler managed to create a  $4.9^\circ\text{C}$  below ambient temperature difference even when  
140 more than  $850\ \text{W}/\text{m}^2$  of solar irradiation was incident. Zhao et al. [18] used a low-cost  
141 radiative cooling metamaterial to cool water to  $10.6^\circ\text{C}$  below ambient temperature.  
142 Nevertheless, despite these significant breakthroughs, the RSC has a low cooling  
143 capacity so it requires large amounts of material to realize building cooling. This issue  
144 is especially detrimental for daytime radiative sky cooling because their required  
145 materials are very specialized and expensive to manufacture [1, 19]. As a result, RSC  
146 is commonly regarded as an uneconomical option for the building cooling application.

147

148 Recently, achieving the RSC and solar thermal functions adaptively with a single panel  
149 (PT-RSC) is another recently emerging technology that aims to maximize the usage of  
150 the panel throughout the day; During the daytime, the panel converts solar energy into  
151 heat, and during the nighttime, the same panel is used to achieve RSC. To achieve this,  
152 Hu et al. [19] proposed a hypothetical solar heating and radiative cooling (SH-RC)  
153 surface and compared it with traditional solar selective absorbing coating surface (SH  
154 surface), spectrally selective radiative cooling surface (RC surface), and spectrally  
155 nonselective black surface (SH-RC<sub>black</sub> surface). Hu et al. [20] later proposed a dual-  
156 function collector with heating during the day and cooling at night, and made a  
157 photothermal radiation cooling model, and carried out experimental research under  
158 heating and cooling modes. Results showed that the collector can get a good daily heat  
159 of 8.64 MJ during a consecutive 8 h and a good nightly cooling energy of 0.99 MJ in a  
160 consecutive 11.5 h. However, the PT-RSC has a major temporal mismatch issue; The  
161 produced daytime heat and nighttime cooling energy are completely opposite to the  
162 typical cooling demand profile of the day, so large and costly thermal storage devices  
163 are generally needed to realize the PT-RSC system's practical potential.



**Figure 1: Ideal emissivity of selectivity coatings**

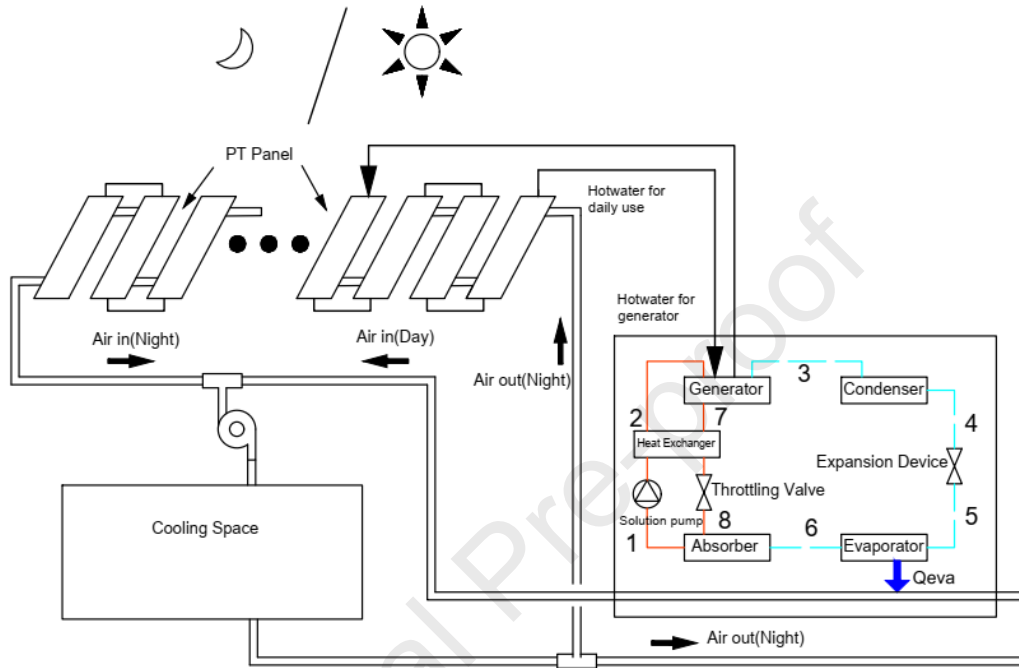
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Although solar absorption chiller (AC) and radiative sky cooling (RSC) have developed maturely, especially AC has been used widely in people's daily life and industry production [21, 22], they still have their shortcomings. In the solar-driven absorption chiller, large energy storage devices are generally required to support nighttime operation and realize 24-h continuous cooling [23, 24]. Otherwise, due to the volatility of solar energy, especially the lack of energy sources at night, other high-grade heat sources may be needed to avoid the situation that the PT-AC system cannot provide nighttime cold energy. In this regard, because the RSC's operation is optimal during the nighttime and does not require additional input energy, its integration into the solar-driven absorption chiller is expected to greatly alleviate the aforementioned drawback. Thus, this paper proposes to combine the RSC with solar-driven AC functions to achieve all-day cooling while reducing the need for thermal storage. During the daytime, PT-AC works to convert solar energy into heat via a heat transfer fluid (HTF), which is later transferred to the AC to produce cooling energy. Then, during the nighttime, the PT panels will be reversed to radiate infrared energy through the bottom layer that is coated with a selective absorbent coating. Compared with the traditional PT-AC and PT-RSC systems that require a thermal storage tank to realize the all-day cooling, the PT-AC-RSC system can reduce the floor space and the initial system equipment investment. In this way, RSC and PT-AC are integrated to avoid preparing separate sites for these two devices, which greatly reduces the demand for land. In addition, the added RSC enabled the new system to better withstand the drastic changes in solar energy and thermal load, thus showing better stability. The proposed system has been studied by analyzing its ability to meet a continuous cooling demand of a typical home in summer conditions. Several system working parameters have been parametrically studied to assess the factors that can enable the highest system performance.

## 191 2.SYSTEM MODELING

192 Figure 2 shows the overall structure of the PT-AC-RSC system, which works differently  
193 between the daytime and nighttime periods. During the daytime, the PT-RSC converts  
194 the solar energy into the heat that drives the AC and ultimately produces cooling energy.

195 When the solar radiation is lower than the driving solar radiation ( $I_d$ ) of AC, the AC  
 196 stops functioning and the RSC takes place to produce cooling energy via infrared  
 197 radiation into the sky. To realize this, the bottom plate is coated with an absorber  
 198 selective material, and the PT panel should be physically rotated 180 degrees because  
 199 this coating causes large heat losses during daytime operation of absorbing solar energy.  
 200 The working process of each model was simulated by MATLAB.



201  
 202 **Figure 2: Schematic of the PT-AC-RSC system**

203 The analyzes are conducted with respect to the time of day and the timestep is set to 1  
 204 hour. To simplify the analysis, it is assumed that the solar irradiation, cooling  
 205 demand/supply, and other working parameters are constant during each hour. In this  
 206 manner, the constant working conditions are inputted to the developed steady-state  
 207 models to calculate the working status and heat flows of the PT-AC-RSC system at each  
 208 time step. These steady-state models are described in detail in the following subsections.

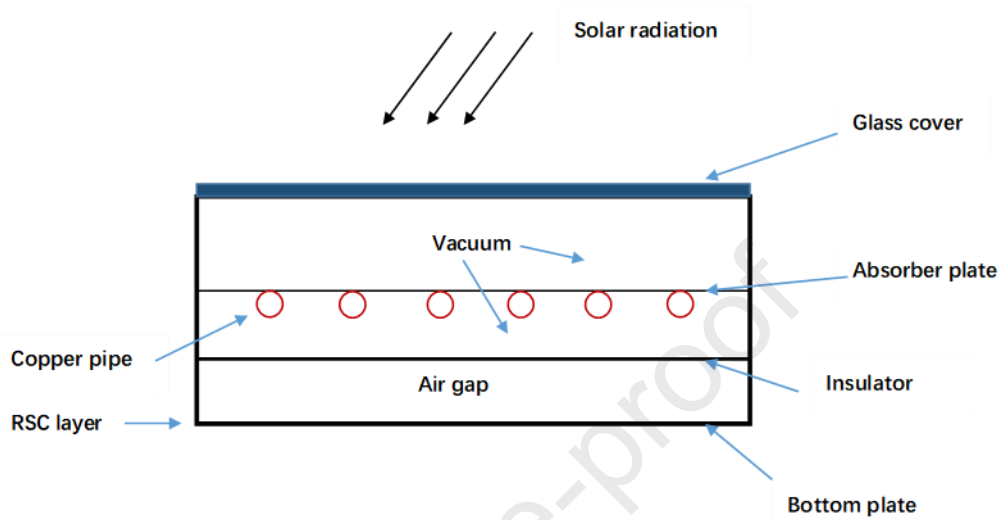
## 209 2.1 Photothermal and radiative sky cooling model

210 Figure 3 shows the structure of the flat plate solar collectors (FPSC) of the PT-RC model.  
 211 From top to bottom, the structure consists of the glass cover, absorber plate, fluid pipe,  
 212 and bottom plate. As the RSC causes problems to the FPSC's solar thermal performance,  
 213 the following measures are imposed on the FPSC.

- 214 1. The coating on the absorber plate has a high absorptivity in the solar band and very  
 215 low emissivity in the other wavelength bands.
- 216 2. The coating on the bottom plate has a very high emissivity in the infrared band,  
 217 especially in the "atmospheric window". When the solar irradiance magnitude is no  
 218 longer sufficient to maintain the AC's operation, the FPSC is flipped 180 degrees  
 219 to make this coating face the sky and initiate the RSC operation.
- 220 3. A vacuum environment is imposed between the glass cover and absorber plate as



- 221 well as between the absorber plate and insulator to reduce heat loss. An air gap also  
 222 exists between the insulator and the bottom plate, which allows the cooling energy  
 223 from the RSC to be carried into the room by flowing air.  
 224 4. It is assumed that the insulator temperature equals the absorber temperature.



225  
226 **Figure 3: Schematic of the EFPC**

### 227 2.1.1 Mathematical model of the photothermal

228 According to the law of energy conservation, the energy used for water heating ( $Q_h$ ) is  
 229 equal to the amount of solar energy ( $Q_s$ ) absorbed minus the heat loss ( $Q_L$ ) of the  
 230 collector to the ambient environment:

$$231 \quad Q_h = Q_s - Q_L \quad (1.)$$

232 where  $Q_L$  includes the heat loss at the top ( $Q_{top}$ ), the heat loss at the side ( $Q_{side}$ ) and  
 233 the heat loss at the bottom  $Q_b$ . Therefore,  $Q_L$  can be expressed as:

$$234 \quad Q_L = Q_{top} + Q_{side} + Q_b = A_{top}U_{top}(T_{abs} - T_{amb}) + A_{side}U_{side}(T_{abs} - T_{amb}) +$$

$$235 \quad A_{bot}U_b(T_{abs} - T_{amb}) \quad (2.)$$

236 Because the average temperature of the absorber plate  $T_{abs}$  is hard to measure, the  
 237 general practice is to introduce the collector efficiency factor  $F'$ , and rewrite the above  
 238 equation into the following form[11]:

$$239 \quad Q_h = A_{abs}F_R[I\tau\alpha - U_L(T_{f,i} - T_{amb})] \quad (3.)$$

240 where:

$$241 \quad F_R = \frac{Mc_p}{A_{abs}U_L} [1 - \exp(-F' A_{abs}U_L/mc_p)] \quad (4.)$$

$$242 \quad F' = \frac{1}{W[\frac{1}{D_0 + (W - D_0)F} + \frac{U_L}{C_b} + \frac{U_L}{\pi D_i h_{f,i}}]} \quad (5.)$$

$$243 \quad F = \frac{\tanh[\frac{U_L}{\sqrt{\lambda_p \delta_p}}(W - D_0)/2]}{\sqrt{\frac{U_L}{\lambda_p \delta_p}}(W - D_0)/2} \quad (6.)$$

244 Here,  $C_b$  is the thermal conductivity at the joint of the tube and plate, which can be

245 calculated by the following formula:

$$246 \quad C_b = \frac{k_b b}{\gamma} \quad (7.)$$

247 where  $b$  and  $\gamma$  are the average width and thickness of the welding material  
248 respectively;  $h_{f,i}$  is the average convective heat transfer coefficient in the tube and can  
249 be calculated by:

$$250 \quad h_{f,i} = (1430 + 23.3(T_{f,m} - 273.15) - 0.048(T_{f,m} - 273.15)^2)V_f^{0.8}D_i^{-0.2} \quad (8.)$$

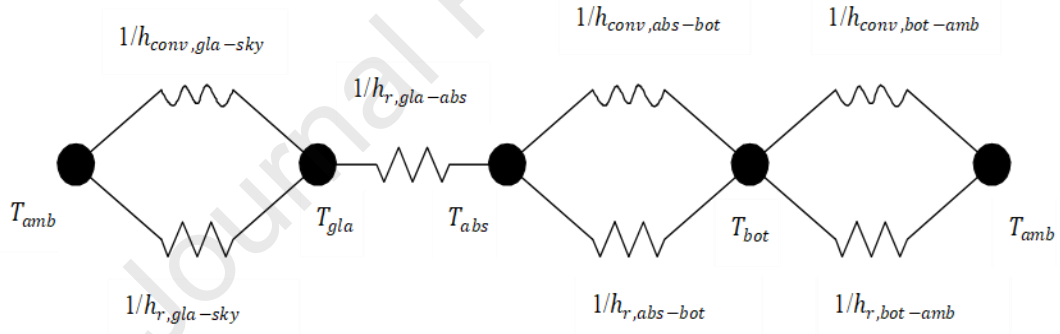
251  $V_f$  is the flow velocity in the tube. The average temperature of the heat transfer fluid  
252 can be obtained by integrating the temperature along the entire length of the pipe and  
253 taking its average. The specific process can be found in [25], and the obtained  
254 expression is:

$$255 \quad T_{f,m} = T_{f,i} + \frac{Q_h/A_{abs}}{F_R U_L} (1 - F_R/F') \quad (9.)$$

256 Therefore, the outlet water temperature of the PT model can be expressed as:

$$257 \quad T_{f,o} = 2T_{f,m} - T_{f,i} = T_{f,i} + 2 \frac{Q_h/A_{abs}}{F_R U_L} (1 - F_R/F') \quad (10.)$$

258 In the above equations,  $U$  is the heat loss coefficient and  $U_L$  means the total heat loss  
259 coefficient. These can be obtained by modeling the system in a thermal resistance  
260 network, which is shown in Figure 4.



261  
262 **Figure 4: The thermal resistance network diagram**

263 The performance of the PT model can be expressed by the thermal efficiency  $\eta_{PT}$  and  
264 its expression is:

$$265 \quad \eta_{PT} = \frac{Q_h}{A_{abs} I} = F_R \tau \alpha - F_R U_L \frac{(T_{f,i} - T_{amb})}{I} \quad (11.)$$

266 The above equations can all be solved after setting the relevant physical parameters of  
267 the FPSC. Doing so yields the outlet water temperature as needed to evaluate the COP  
268 of the AC and the thermal efficiency of the PT model.

### 269 **2.1.2 Mathematical model of the radiative sky cooling**

270 The PT-RSC model reverses at night so that the bottom faces up for radiative cooling,  
271 and the thermal balance of night radiative sky cooling is shown in Figure 5. The net  
272 radiative sky cooling power  $Q_{net,rad}$  can be calculated as follows (taken from [10,  
273 26]):

$$274 \quad Q_{net,rad} = Q_{rad} - Q_{r,atm} - Q_{c,atm} - Q_s \quad (12.)$$

275 where  $Q_{rad}$  is the thermal radiation energy;  $Q_{r(atm)}$  is the returned radiation energy

276 from the atmosphere; They can be respectively expressed as:

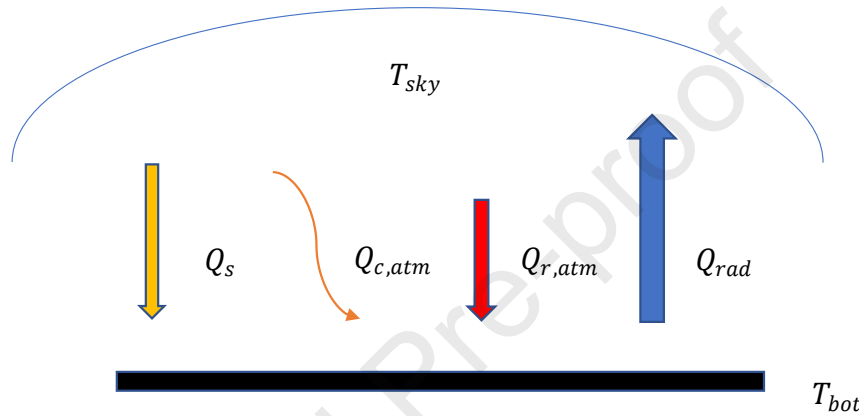
$$277 \quad Q_{rad} = \int \cos\theta d\Omega \int I_{bb}(\lambda, T_s) \varepsilon_s(\Omega, \lambda) d\lambda \quad (13.)$$

278 and:

$$279 \quad Q_{r,atm} = \int \cos\theta d\Omega \int I_{bb}(\lambda, T_{amb}) \varepsilon_s(\Omega, \lambda) \varepsilon_{atm}(\Omega, \lambda) d\lambda \quad (14.)$$

280  $Q_{c,rad}$  is convective heat transfer with the ambient air, and  $Q_s$  is the absorbed solar irradiation power on the surface. Therefore,  $Q_{net,rad}$  can be further expressed as:

$$282 \quad Q_{net,rad} = A_{bot}[\varepsilon\sigma(T_b^4 - T_{sky}^4) + h(T_b - T_{amb}) - \alpha_s I] \quad (15.)$$



283

**Figure 5: The thermal balance of night radiative sky cooling**

284 where  $T_{sky}$  is the effective sky temperature. The researchers have developed some  
 285 models for calculating the effective sky cooling under clear sky[27, 28]. In this paper,  
 286  $T_{sky} = 255K$  is imposed, which is consistent with that used in Bergman's work[26].  
 287  $I$  is the solar radiation intensity. In the simulation of this paper, the value of  $I$  is the  
 288 solar radiation intensity of Hefei in the first week of August obtained from  
 289 EnergyPlus[29].

291 The convection heat transfer coefficient between the bottom and the ambient is often  
 292 calculated by the following formula [11]:

$$293 \quad h = 5.8 + 3.8V_{wind} \quad (16.)$$

294 Notably, one may choose to install a convection shield over the radiative cooling  
 295 surface to minimize the side effect of convective heat transfer. For example, the RSC  
 296 module was covered with polyethylene film, a concept proposed by Zhao et al. [30] that  
 297 changed the heat transfer coefficient to become:

$$298 \quad h = 2.5 + 2.0V_{wind} \quad (17.)$$

299 Meanwhile, because the coating of the PT's bottom layer has a high emissivity on the  
 300 infrared band, the heat loss between the ambient and bottom plate will be higher under  
 301 the same temperature difference compared with the traditional PT panel. Hence, it is  
 302 required that the thermal resistance between absorber and bottom plate be maximized,  
 303 which is dependent on the heat transfer coefficient  $h_{bi}$  between the bottom and  
 304 insulative layers. This parameter is mainly determined based on the thickness of the air  
 305 gap:

$$306 \quad h_{bi} = \frac{k}{d_{air}} \quad (18.)$$

307 where  $k$  is the thermal conductivity of air and  $d_{air}$  is the thickness of the air gap. For  
 308 convenience, an idealized spectrally selective surface shown in Figure 1 is assumed for  
 309 the bottom layer [31]. Specifically, the surface has a high emissivity  $\varepsilon_s = 0.95$  only  
 310 at long wavelengths ( $\lambda > 2.5\mu m$ , which includes the atmospheric window,  $8\mu m <$   
 311  $\lambda < 13\mu m$ ) while  $\varepsilon_s = 0$  at short wavelengths ( $\lambda < 2.5\mu m$ ). Therefore, the total  
 312 emissivity  $\varepsilon$  of the bottom surface, at the temperature  $T_b$  is [32]:

$$313 \quad \varepsilon_{T_b} = \frac{\int_0^{\infty} \varepsilon_{\lambda}(\lambda, T_b) E_{\lambda, b}(\lambda, T_b) d\lambda}{E_b(T_b)} = \frac{\int_0^{2.5\mu m} \varepsilon_s E_{\lambda, b}(\lambda, T_b) d\lambda}{E_b(T_b)} \\ 314 \quad + \frac{\int_{2.5\mu m}^{\infty} \varepsilon_s E_{\lambda, b}(\lambda, T_b) d\lambda}{E_b(T_b)} \quad (19.)$$

## 315 2.2 Mathematical model of absorption chiller

316 Figure 2 additionally shows the structure of the single effect lithium-bromide  
 317 absorption chiller (AC) whose operating principle is summarized as follows:

- 318 (1) The concentrated solution in the generator will be heated by hot water from the  
 319 solar collectors. The obtained refrigerant with high temperature and high pressure  
 320 becomes liquid after passing through the condenser.
- 321 (2) After the refrigerant passes through the expansion device and becomes liquid at low  
 322 temperature and low pressure, it provides cooling energy to the flowing cold air.
- 323 (3) Finally, the refrigerant returns to the absorber to be recombined with the solution,  
 324 which is then pumped to the generator.
- 325 (4) There is a heat exchanger between the generator and the absorber. The heat  
 326 exchange between the concentrated solution and the dilute solution improves the  
 327 efficiency of energy utilization.

328 According to the first law of thermodynamics:

$$329 \quad Q_{eva} + Q_{gen} = Q_{con} + Q_{abs} \quad (20.)$$

330 The energy balance at the generator yields the following equation:

$$331 \quad Q_{gen} = \dot{m}_3 h_3 + \dot{m}_7 h_7 - \dot{m}_2 h_2 \quad (21.)$$

332 The COP of the solar absorption chiller can be calculated as:

$$333 \quad COP = \frac{Q_{eva}}{Q_{gen}} \quad (22.)$$

334 where  $Q_{gen}$  is the input heat into the AC;  $\dot{m}$  is the mass flow rate (kg/s) of the  
 335 solution or the water,  $h$  is the specific enthalpy of the working medium. For the salt  
 336 solution,  $h$  can be calculated according to the reference [26]:

$$337 \quad h_i = (0.0976X_j^2 - 37.512X_j + 3825.4)T_i \quad (23.)$$

338 where  $X$  and  $T$  are the mass fraction and temperature of the solution, respectively.  
 339 According to the ASHRAE Handbook 2013 [33], the evaporation temperature can be  
 340 obtained in terms of different mass concentrations and pressures of lithium bromide  
 341 aqueous solutions:

$$342 \quad T = A_0 + A_1 \ln P + A_2 (\ln P)^2 + A_3 (\ln P)^3 \quad (24.)$$

343 In the formula,  $P$  is the saturated vapor pressure of LiBr-H<sub>2</sub>O and the coefficients  $A_0$ ,

344  $A_1, A_2, A_4$  are:

$$\begin{aligned}
 345 \quad A_0 &= a_0 + a_2X + a_4X^2 + a_7X^3 \\
 346 \quad A_1 &= a_1 + a_5X + a_9X^2 \\
 347 \quad A_2 &= a_3 + a_8X \\
 348 \quad A_3 &= a_6 \quad (25.)
 \end{aligned}$$

349 Coefficients  $a_0, a_1 \dots a_9$  are regression coefficients obtained by the least-squares  
 350 regression method respectively, and their values are shown in Table 1.

351 **Table 1: The coefficient values of Equation (22)**

<b>n</b>	<b><math>a_n</math></b>	<b>n</b>	<b><math>a_n</math></b>
0	34.33	5	-16.42
1	18.27	6	0.1108
2	-180.0	7	42.52
3	0.4172	8	0.9320
4	360.1	9	23.10

352 As for water, the specific enthalpy can be calculated by using a thermophysical  
 353 properties calculation package such as CoolProp [25]. Thus, the cooling energy  
 354 produced by AC can be expressed as:

$$355 \quad Q_{eva} = \dot{m}_6(h_6 - h_5) \quad (26.)$$

356 In this paper, we first designed an AC model with a rated power of 14 kW. The relevant  
 357 design parameters are shown in Table 2.

358 **Table 2: Design parameters of AC**

<b>Parameters</b>	<b>Value</b>
Rated power	14kW
The inlet temperature of the heat source water	100°C
The inlet temperature of cooling water	31°C
Chilled water inlet and outlet temperature	12°C, 7°C

### 359 **2.3 Solving the system model**

360 For daytime cooling, when the basic physical parameters such as local total solar  
 361 radiation  $I$ , the inlet water temperature of PT model  $T_{PT,in}$ , wind speed  $V_{wind}$ , ambient  
 362 temperature  $T_{amb}$  are known, the outlet temperature and the cooling energy of the AC  
 363 can be calculated. This is achieved by the following procedure:

364 1. Input the known parameters, including  $T_{PT,in}$ ,  $I$ ,  $V_{wind}$  et al into the PT model to

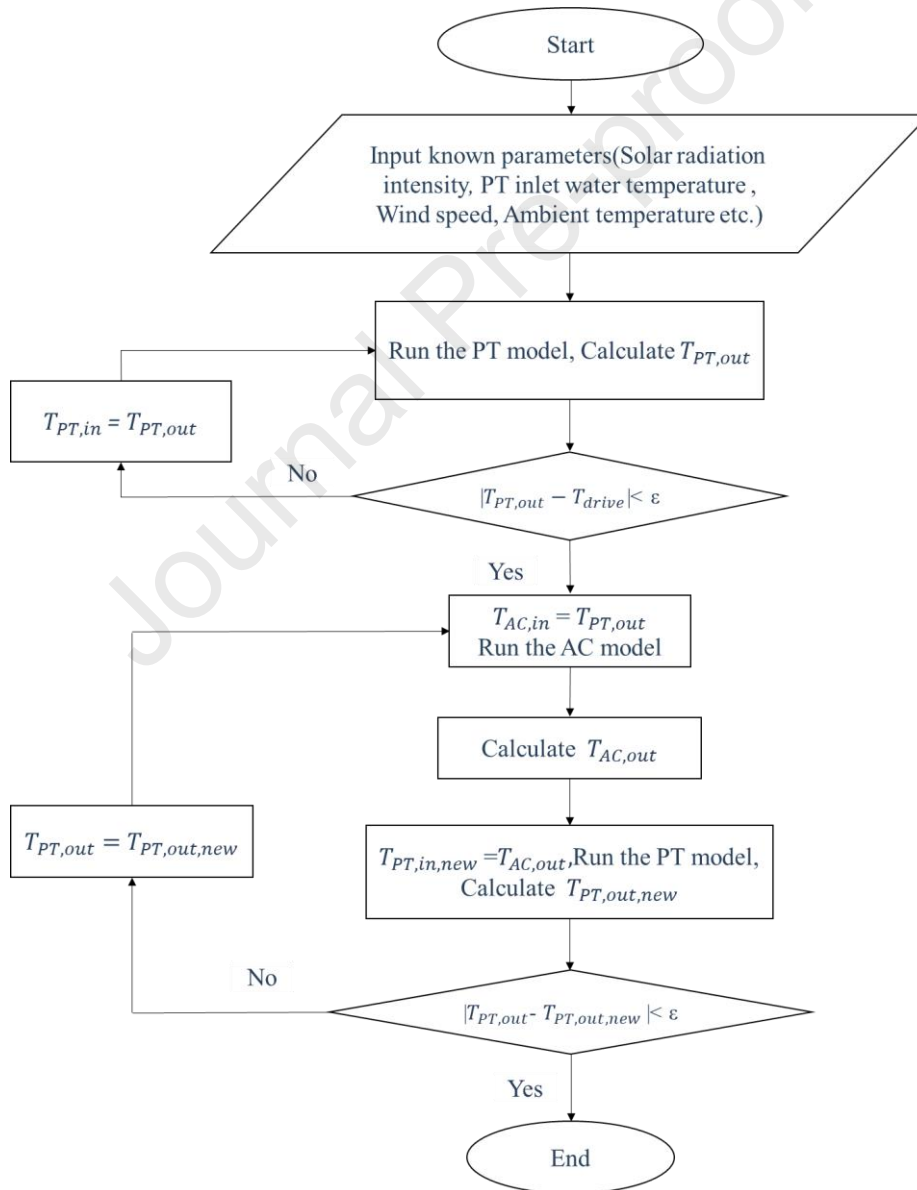
- 365 obtain PT outlet water temperature  $T_{PT,out}$ .
- 366 2. Determine whether  $T_{PT,out}$  reaches the AC driving temperature  $T_{drive}$ . If so, go to
- 367 step 3, otherwise, return to step 1.
- 368 3. Run AC model to obtain the AC outlet water temperature  $T_{AC,out}$ .
- 369 4. Take  $T_{AC,out}$  as the new PT inlet water temperature  $T_{PT,in,new}$ , and run the PT
- 370 model to obtain the new PT outlet water temperature  $T_{PT,out,new}$ .
- 371 5. Compare  $T_{PT,out,new}$  with  $T_{PT,out}$ , if  $T_{PT,out}$  converges, the program terminates,
- 372 otherwise, go back to step 3.

373 A numerical simulation program of the model is developed on MATLAB, and the

374 calculation process is summarized in Figure 6. The efficiency of the PT-AC system can

375 be summarized as:

$$376 \quad \eta_{total} = \frac{Q_E}{A_{abs}I} = \frac{Q_h}{A_{abs}I} \frac{Q_E}{Q_G} = \eta_{PT} COP \quad (27.)$$



377

378

Figure 6: Flow chart of the calculation process for the PT-AC system.

## 379 2.4 Thermal load model

380 To evaluate the performance of the system, a simplified building model is designed to  
 381 calculate its thermal load, which is later used as the basis for designing the proposed  
 382 cooling system. The relevant parameters are shown in Table 3.

383 **Table 3: Parameters of the building space**

Parameters	Value
Room dimensions	3.5 m (height) x 10 m (length) x 7 m (width)
Corresponding wall area ( $A_{wall}$ ), floor area ( $A_{floor}$ ) and volume of the room ( $V_{room}$ )	119 m <sup>2</sup> , 70 m <sup>2</sup> , and 245 m <sup>3</sup> , respectively
Area of window ( $A_{win}$ ) that faces south	1.5 m (length) × 2 m (width) × 3 m <sup>2</sup>
The heat transfer coefficient of floor ( $U_f$ )	1.5W/(m <sup>2</sup> · K)

384 Based on the thermal load model by Khammayom et al. [34], the thermal load  $Q_L$  of  
 385 the room without radiation can be calculated as:

$$386 \quad Q_L = U_f A_{floor} (-0.3099T_{room} + 0.3867T_{amb}) \quad (28.)$$

387 whereas in the daytime, the heat load will be affected by solar radiation through the  
 388 window. Therefore, we can express  $Q_L$  approximately as:

$$389 \quad Q_L = U_f A_{floor} (-0.3099T_{room} + 0.3867T_{amb}) + \tau_{win} A_{win} I_{v,dir} \quad (29.)$$

390 where  $\tau_{win}$  is the transmittance of the window and is set as 0.95,  $I_{v,dir}$  is the incident  
 391 direct solar irradiation that is perpendicular to the vertical surface. Taken from [35],  
 392  $I_{v,dir}$  can be expressed as follows:

$$393 \quad I_{v,dir} = \frac{I_{m,dir} \cdot \cos(\theta)}{\cos(\theta_z)} \quad (30.)$$

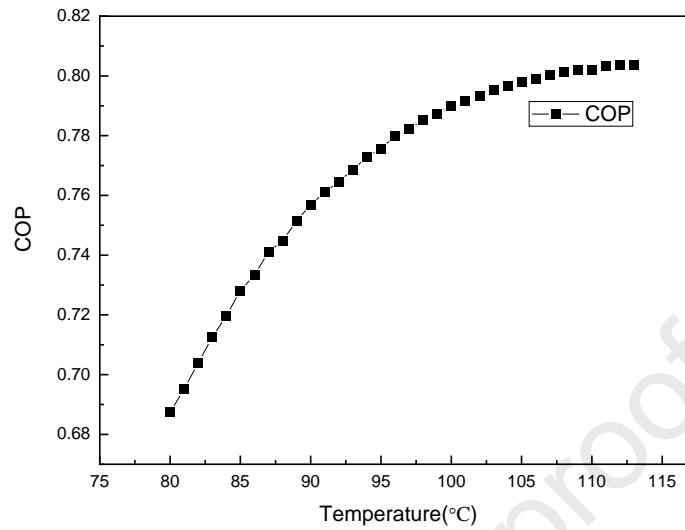
394 where  $I_{m,dir}$  means measured direct solar irradiation (perpendicular to the ground),  
 395  $\theta_z$  and  $\theta$  represent the angle between the sun's rays and the normal of the ground and  
 396 vertical surfaces, respectively. These angles can be calculated from the local latitude  
 397 and longitude, solar time, etc.

## 398 3. MODEL VALIDATION

### 399 3.1 Absorption chiller model validation

400 The AC model is executed to yield COP results which will be verified in terms of  
 401 accuracy. Here, the evaporation temperature is 5°C, cooling water temperature of 35°C,  
 402 and condensation temperature of 40°C. The results are shown in Figure 7, which shows

403 that the COP increases from 0.6 to 0.8 as the generation temperature varied from 80□  
 404 to 110°C. Figure 7 shows the temperature and COP of the single effect absorption chiller.



405

406 **Figure 7: Daily performance of the absorption chiller.**

407 The validation of the AC model is performed with Miao et al. [36], and the comparative  
 408 results are shown in Table 4. From the chosen five different hot water temperatures, we  
 409 can see that a good agreement proves that the present model is valid and accepted. Since  
 410 the model's designed generator temperature is 100°C, which is larger than in the  
 411 reference, the error gradually increases as the temperature increases.

412

**Table 4: Validation result of AC model**

Hot water temperature	COP from Ref.[36]	COP from the present model	Error (%)
85	0.7156	0.7281	1.72
87	0.72772	0.74103	1.80
90	0.73827	0.7569	2.46
92	0.74388	0.76865	2.90
95	0.74568	0.7757	3.87

### 413 3.2 Radiative sky cooling model validation

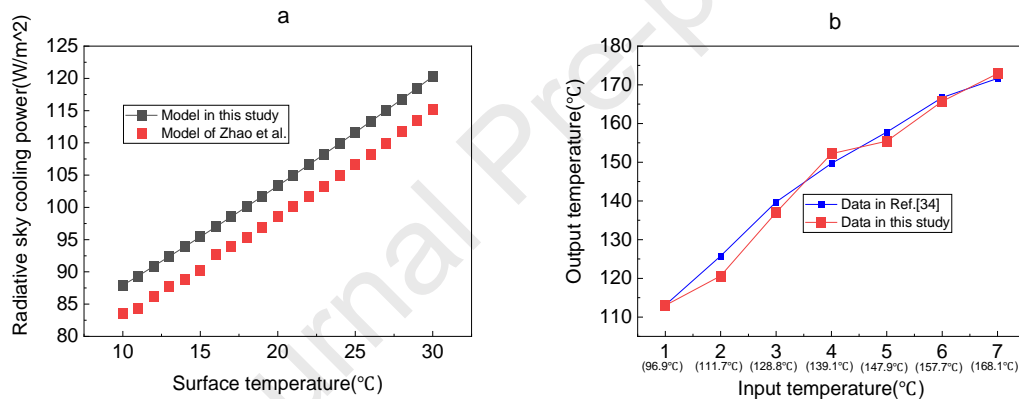
414 Zhao et al.[10] calculated and tested the net radiation heat flux of selective surface for  
 415 various surface temperatures. In their study, all tests were under the condition that the  
 416 surface temperature is close to the ambient temperature to eliminate the convective and  
 417 conductive heat transfer between the radiative cooling surface and the ambient. These  
 418 same conditions have been applied to our model from Section 2.1, and the comparison



419 of the results with Zhao et al. is shown in Figure 8 (a). The error between the two may  
 420 be due to differences in atmospheric transmittance. But overall, the comparison shows  
 421 that the model in this paper is in good agreement with the references. The average  
 422 relative error is about 5.36%, therefore, we believe that the RSC model in this study is  
 423 reliable and accurate.

### 424 3.3 Photothermal model validation

425 Gao et al.[37] has carried out an experimental study on the related properties of the  
 426 evacuated flat plate collector. In their study, a medium-scale thermal system was used  
 427 to obtain the output water temperature at different input water temperatures and solar  
 428 irradiation with the ambient temperature of 35.7°C. Under the same working conditions,  
 429 and assuming that there is no air gap, we simulated the PT model mentioned in section  
 430 2.1. The simulation results and the experimental results of Ref.[37] are all shown in  
 431 Figure 8 (b). The results show that the PT model is reliable.  
 432



433  
 434

**Figure 8: The validation of RSC model (a) and the validation of PT model (b)**

## 435 4. RESULT AND DISCUSSION

436 The PT-AC-RSC system has been simulated under varying ambient conditions of the  
 437 day, and the produced cooling energy is compared with the cooling demand of the  
 438 building room to evaluate their temporal matching characteristics. First, an analysis  
 439 using a typical scenario is conducted, which will reveal that the daytime cooling  
 440 demand is more than that available if the PT-RSC device is sized to exactly meet the  
 441 nighttime cooling demands. Hence, the performance of the system with a thermal  
 442 storage tank is evaluated and compared with the traditional PT-AC system. By  
 443 recognizing the PT-AC-RSC system performs unusually poorly at the sunrise and  
 444 sunset periods, methods to mitigate the poor performance at these times are proposed  
 445 and analyzed. Finally, the stability of the PT-AC-RSC system under multiple days with  
 446 different weather conditions is conducted.

#### 447 **4.1 Preliminary analysis**

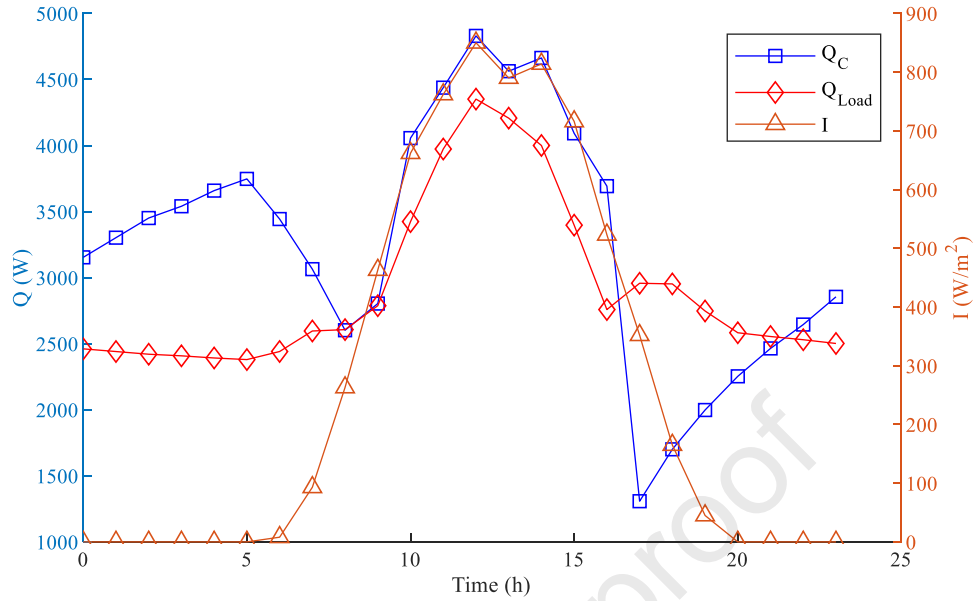
448 Base case results are reported below, where the cooling space temperature ( $T_{room}$ ) is  
449 first fixed at the target of 27°C, and the ambient temperature, ambient RH, and  
450 magnitude of solar irradiance are all varied according to Hefei's weather data on August  
451 1. The area of the PT panel is assumed to be  $A_s = 30 \text{ m}^2$ . It is assumed that the surface  
452 temperature of the PT plate is almost equal to room temperature ( $T_s \approx T_{room}$ ) when the  
453 system is operating in RSC mode. The convective heat-transfer coefficient  $h_{bi}$   
454 between the absorber and bottom plates is set as  $1 \text{ W}/(\text{m}^2 \text{ K})$  at daytime, that is, the  
455 air gap is set as 3 cm.

456  
457 The all-day cooling energy is shown in Figure 9, including the radiation sky cooling  
458 energy at night and the absorption chiller cooling energy at daytime. Clearly, the cooling  
459 energy of RSC is about  $50\sim 100 \text{ W}/\text{m}^2$  and depends on the ambient temperature. In the  
460 daytime, the cooling capacity of the AC varies with a similar trend to that of the solar  
461 radiation intensity, which first increases and then decreases. There are periods in the  
462 sunrise and sunset in which the cooling capacity of the system is low. These periods  
463 shall be named the "Alternating period of refrigeration (APR)". During these times,  
464  $T_{amb}$  is too high and there's too much convective heat loss. Meanwhile, the PT panel  
465 will inevitably absorb some solar radiation. However, at the same time, the solar  
466 radiation is also too weak to heat the water to the required driving temperature by the  
467 AC. Therefore, we can find that the cooling capacity of the RSC at sunset is lower than  
468 that at sunrise because of higher solar irradiation and ambient temperature.

469  
470 By the heat load model mentioned in section 2.4, we also simulated the heat load on  
471 August 1 based on Hefei's weather data.  $I$  is the solar radiation density. The  
472 calculation results of all-day thermal load are also shown in Figure 9. These results  
473 indicate that the cooling energy generated by the new system is roughly equal to an  
474 entire day's heat load. Among them, the AC model performs very well, showing  
475 sufficient cooling capacity. However, during the sunset, the cooling capacity of daytime  
476 RSC is somewhat inadequate because the ambient temperature is still very high to cause  
477 a high thermal load and low cooling capacity of RSC. Hence, the APR is a very  
478 significant problem and a more detailed analysis shall be conducted in Section 4.2 to  
479 find solutions to reduce its impact on the time of insufficient cooling capacity.

480

481



482

483 **Figure 9: Cooling energy of PT-AC-RSC system and heat load with the time on August 1**

484

## 4.2 Solutions to reduce the alternating period of

485

### refrigeration

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491

As shown by the analysis in Section 4.1, the presence of the APR problem is bound to affect human comfort. This problem can be solved by considering two aspects. The first is to increase the output water temperature  $T_{f,o}$  by improving the thermal efficiency  $\eta_{PT}$  of the PT device. Due to the heat transfer coefficient  $h_{bi}$  is a very important influential factor on the PT panel's thermal efficiency, so methods to minimize it will be determined.

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### 4.2.1 Influence of heat transfer coefficient $h_{bi}$

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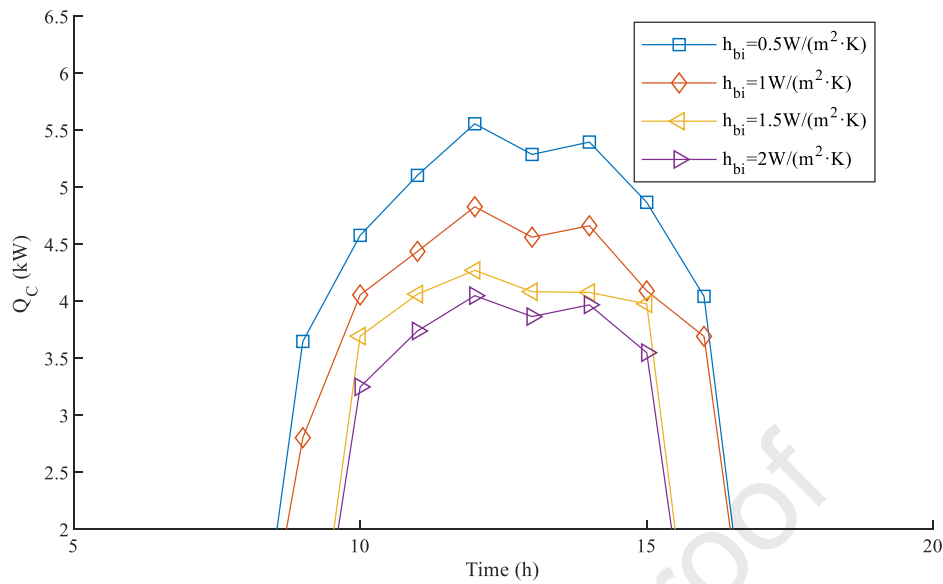
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The solar radiation intensity is first simulated based on the summer solstice in Hefei. Under this condition, the effect of  $h_{bi}$  is analyzed, which is equivalent to adjusting the air gaps between the components. As shown in Figure 10, the PT-RSC devices with different heat-transfer coefficient  $h_{bi}$  have different cooling capacities. Specifically, at the same irradiation intensity  $I$ , the PT-RC device with low heat transfer coefficient  $h_{bi}$  can get more cooling energy. On one hand, the PT device has higher thermal efficiency due to the reduction of convective heat loss. On the other hand, because of that, the PT device can attain a higher output temperature  $T_{f,o}$ , which can also improve the COP of the AC device. This conclusion is consistent with the trends expected from Eq. (26). Similarly, due to the improvement of the system's thermal efficiency, the outlet water temperature of the PT device also reached the driving temperature of AC earlier, thereby reducing the ARP.

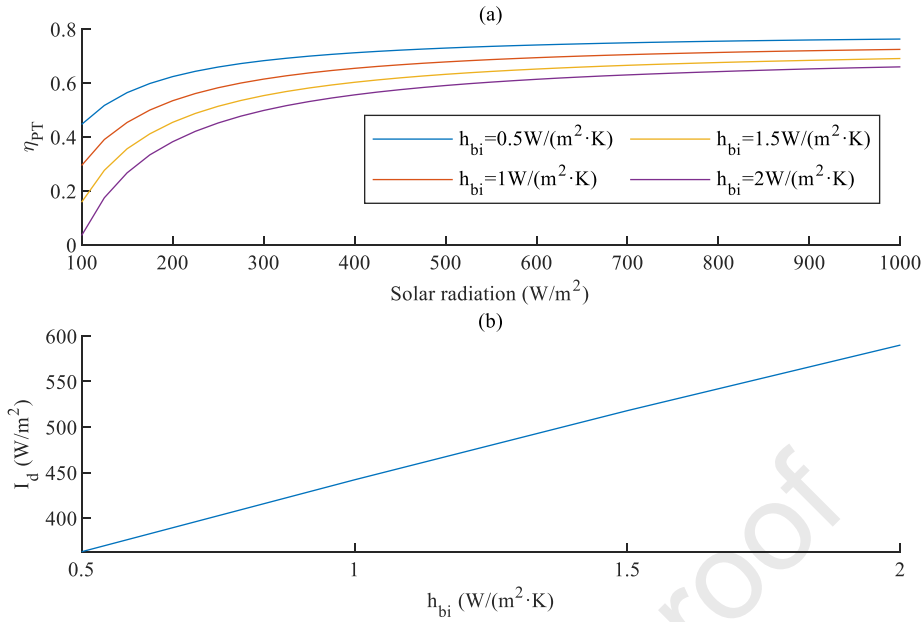


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506

**Figure 10: Cooling energy of PT-AC system with different  $h_{bi}$**

507 More specific details are shown in Figure 11, where Figure 11 (a) shows the thermal  
 508 efficiency of the PT device (PT inlet water temperature equals the ambient temperature)  
 509 and the driving solar radiation intensity ( $I_d$ ) of AC (b) under different  $h_{bi}$ . From Figure  
 510 11 (a), the PT device with lower  $h_{bi}$  has a higher  $\eta_{PT}$  under the same solar radiation  
 511 intensity, especially when the solar radiation intensity is relatively low. From Figure 11  
 512 (b), when  $h_{bi}$  reaches  $2 \text{ W}/(\text{m}^2 \cdot \text{K})$ , the PT device requires a solar radiation of  
 513  $584 \text{ W}/\text{m}^2$  to heat water to driving temperature. The higher  $h_{bi}$  is, the higher solar  
 514 radiation intensity is needed to drive the AC device. The cutoff solar radiation intensity  
 515 shows a linear relationship with  $h_{bi}$ . The driving solar radiation is  $356 \text{ W}/\text{m}^2$  when  
 516  $h_{bi}$  is equal to  $0.5 \text{ W}/(\text{m}^2 \cdot \text{K})$ . This means that at sunrise and sunset, when  $h_{bi}$  is  $0.5$   
 517  $\text{ W}/(\text{m}^2 \cdot \text{K})$  compared with  $2 \text{ W}/(\text{m}^2 \cdot \text{K})$ , the working time of the PT-AC device  
 518 can be increased by about 60 minutes. Considering that the data here is discontinuous,  
 519 the value will be larger.



520

521

**Figure 11: Thermal efficiency  $\eta_{PT}$  of PT-AC system (a) and the cut-off solar radiation intensity of AC (b) with different  $h_{bi}$**

522

523

Although the above results indicate that a smaller  $h_{bi}$  allows a higher PT performance, but a smaller  $h_{bi}$  also means the air gap size would need to be larger, which subsequently increases the PT-RSC panel volume and increases its economic cost. Hence, a value of  $h_{bi} = 0.5 W/(m^2 \cdot K)$  is treated as the most reasonable choice and will be used in the next analyzes. Notably, the effect of a low  $h_{bi}$  value on the RSC performance is an irrelevant study because, during the nighttime, a blower will be used to enable continuous high airflow rate through the PT-RSC panel, which means the practical  $h_{bi}$  value would become significantly high.

529

530

531

#### **4.2.2 Effect of convective heat transfer coefficient on radiative sky**

532

##### **cooling**

533

Except decrease the  $h_{bi}$  to increase the working time of the PT-AC device, the influence of APR can also be reduced by increasing the cooling energy of the RSC device at night time. Here, the convection heat transfer coefficient between the bottom and the environment is known to be the most influential factor.

536

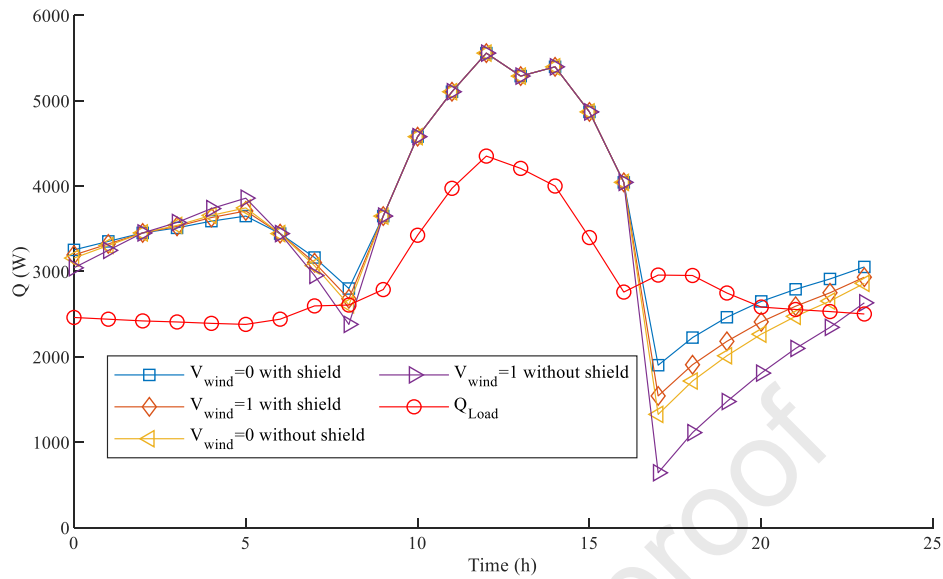
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As Figure 12 shows, the cooling energy produced by four cases were analyzed: shielded and windless (case 1), shielded and the velocity of wind is  $1m/s$  (case 2), without shield and windless (case 3), without shield and  $V_{wind} = 1m/s$  (case 4). The results shows that the convection heat transfer coefficient has a major impact on the RSC cooling capacity especially when the ambient temperature is very high. Equation 15 also proves this. In addition, when it is windless and the shield is taken, the APR is reduced by nearly two hours over case 3. Therefore, in the actual situation, measures are needed (such as covering the PE membrane) to reduce the convective heat transfer

545

546 coefficient as much as possible and ultimately reduce the impact on the RSC.



547

548 **Figure 12: Effects of the different velocity of wind and occlusion measures on system**  
 549 **performance**

## 550 4.3 The system with storage tank

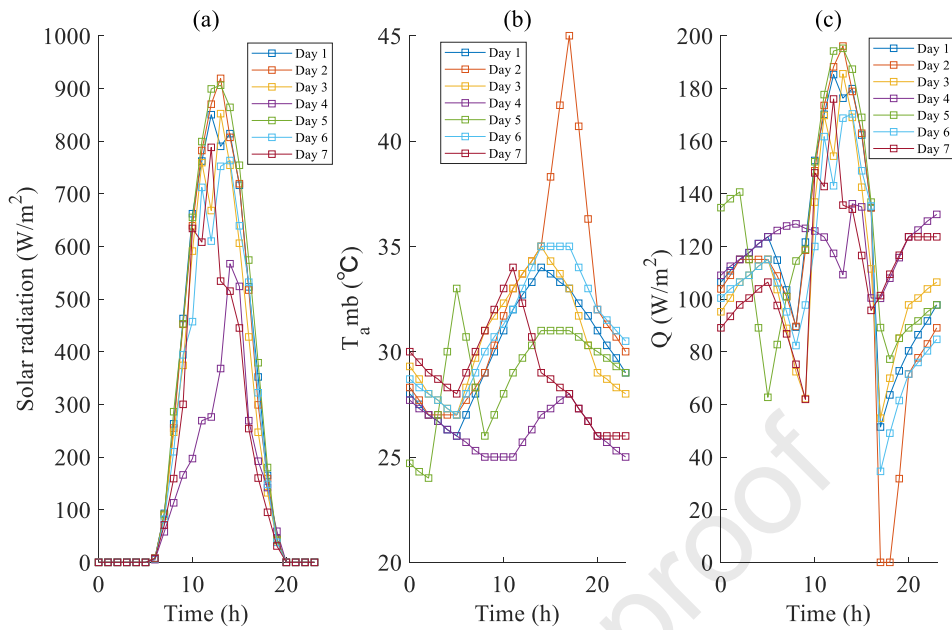
### 551 4.3.1 The energy budget of the system

552 As analyzed above, it is very difficult to completely eliminate the issue under the given  
 553 cooling area and heat load, which is related to the principle of the RSC itself: The  
 554 cooling capacity is negatively correlated with the ambient temperature. Similarly, the  
 555 cooling capacity from dawn to sunrise exceeds the thermal load because of the lower  
 556 ambient temperature. Therefore, in this section, we analyzed the system with a thermal  
 557 storage tank and compared it with a separately PT-AC system. The result shows that  
 558 the new system requires smaller tanks and has greater stability.

559

560 Figure 13 shows the solar radiation intensity, the ambient temperature, and cooling  
 561 capacity of the system for each day of the first week of August, Hefei. Here,  $h_{bi}$  is set  
 562 to  $0.5 \text{ W}/(\text{m}^2 \cdot \text{K})$ , assumed that the RSC device was covered with shield and  $V_{wind}$   
 563 equals to  $1 \text{ m/s}$ . The trend of system cooling capacity is consistent as mentioned above.  
 564 Notably, at 5 pm on Day 2, there was an unusually high temperature, which directly  
 565 caused the RSC to fail to cool.

566



567

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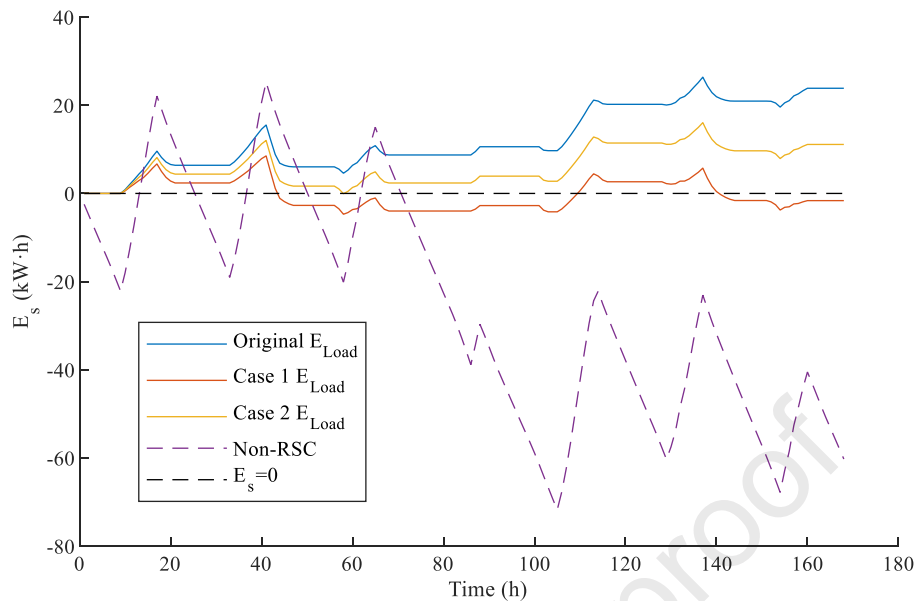
**Figure 13: Weather parameters and cooling capacity for one week: solar radiation (a), ambient temperature (b), cooling energy of the system (c)**

569

570

571 Consider that the cooling energy produced by AC can be stored as chilling water, it is  
 572 more convenient and efficient to use than the cooling air produced by RSC. Therefore,  
 573 it is assumed that only the excess cold energy of AC is stored for use when the cold  
 574 energy is insufficient. From Figure 14, the amount of stored energy is shown to increase  
 575 under the original heat load. There is a significant decrease only in about the 40th hour,  
 576 which is consistent with previous studies. Under the 1.05 times heat load (Case1  $E_{Load}$ ),  
 577 the system can still ensure that the stored energy is always in surplus. At 1.1 times of  
 578 heat load (Case2  $E_{Load}$ ), the energy storage of the system for one week is balanced.  
 579 Hence, for the original heat load, we consider that the scale of refrigeration is  
 580 appropriate.

581



582

583

Figure 14: Energy budget of the system in one week.

584

### 585 4.3.2 System performance stability analysis

586 According to the analysis in section 4.3.1, the new system with a thermal storage  
 587 capacity of 11.5Kw·h of cooling energy is designed. When the radiation cooling energy  
 588 can meet the heat load, only the RSC device works. Otherwise, the system will apply  
 589 the stored cooling energy to satisfy the remaining cooling demands.

590

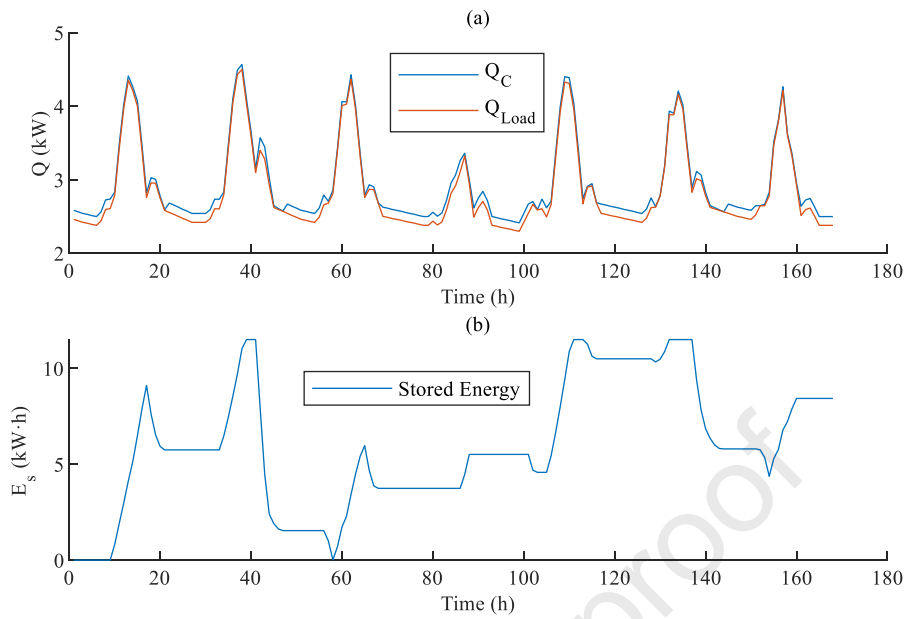
591 Figure 15 (a) shows the cold energy demand of the building and the cooling capacity  
 592 of the system over the seven days. Here, a surplus of 5% of the cooling abundance for  
 593 each moment is reserved. The result shows that cooling energy can fit the heat load well.  
 594 The energy change process of the storage has also been shown in Figure 15 (b). It  
 595 showed that the stored cooling energy is abundant except on day 2 because the high  
 596 temperatures that afternoon caused a large heat load.

597

598 We also compared the performance of the new system with a separate PT-AC system.  
 599 The scale of the PT device is redesigned to make sure that the AC cooling energy can  
 600 satisfy the all-day cooling demand on a sunny day. The energy budget of PT-AC system  
 601 was also shown in Figure 14 (Non-RSC). It showed that the PT-AC system has much  
 602 larger energy fluctuations. Besides that, cloudy weather can cause a huge drain on the  
 603 energy in the tank without replenishment. The PT area and the scale of the storage tank  
 604 of the two systems are shown in Figure 16. One thing to note is that the PT-AC system  
 605 does not consider cloudy weather. In fact, the storage tank size is required to meet the  
 606 maximum energy consumption process of the system. Hence, we can say that the new  
 607 system can use a smaller storage tank and less floor space to get a more stable



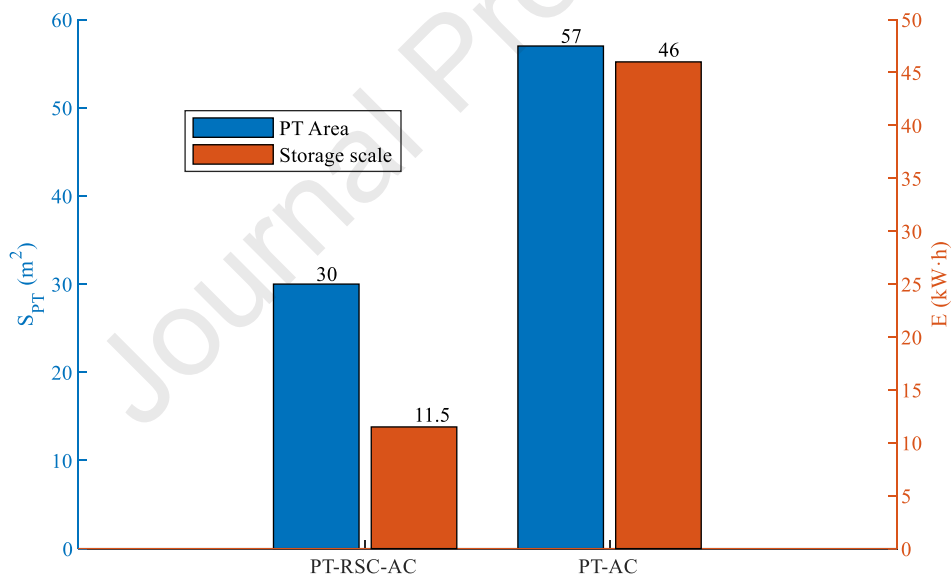
608 refrigeration performance according to the above analysis.



609

610

Figure 15: System cooling capacity and building cooling demand for one week



611

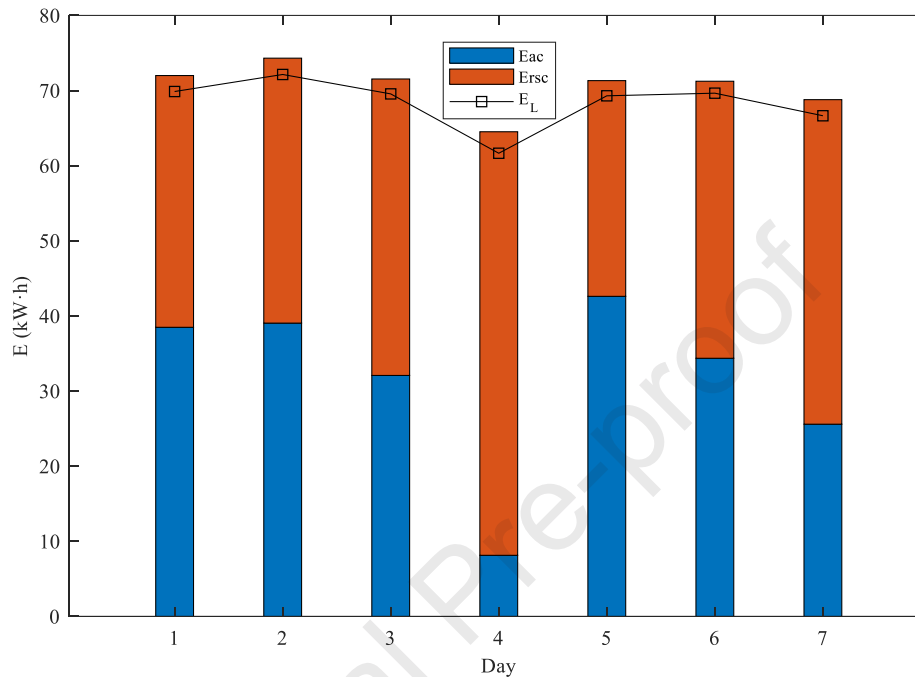
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Figure 16: PT area and storage tank scale of PT-AC-RSC system and PT-AC system

### 613 4.3.3 Energy analysis

614 For a more comprehensive evaluation of system performance, the energy output is  
 615 analyzed for seven days. As shown in Figure 17 the cooling capacity of RSC and AC  
 616 are similar in quantity. This occurred because the RSC has a much longer working time  
 617 compared with the AC device. However, there is a huge decrease in AC cooling capacity  
 618 on day 4. As Figure 13 (a) shows, the solar irradiation on day 4 is lowest this week, so  
 619 it was estimated that the day might be overcast or cloudy. In contrast, the  $E_{RSC}$  is

620 extremely high because of the cooler temperatures of day 4. Therefore, the total cooling  
 621 energy is relatively adequate compared with heat load on day 4 from Figure 17. It also  
 622 proved the advantage of the new system: it is more stable to avoid the problems caused  
 623 by the scarcity of AC cooling capacity. Except for this, the all-day cooling energy  
 624 matched well with the heat load.



625  
 626  
 627

Figure 17: Energy output for one week

## 628 5. CONCLUSION

629 This paper proposed a new all-day cooling system that combined PT-AC with RSC.  
 630 Based on the vacuum flat plate solar collector, a reversible PT plate with selective  
 631 absorption coating on the bottom was proposed. This method can significantly reduce  
 632 the space demand and tank size of the PT-AC system, and improve the economic benefit.  
 633 In addition, we also find that the new system is more stable and less affected by solar  
 634 energy fluctuations. More specifically, during the daytime, this new system works like  
 635 a traditional solar absorption chiller. But at nighttime or when solar radiation is low,  
 636 such as sunrise and sunset, the PT panels are rotated around to radiate infrared energy  
 637 for cooling. After simulating this new system via a time-dependent simulation that  
 638 assumes steady-state characteristics during each hour of the day, it is revealed that:

- 639 1. The new system can meet the cooling needs of Hefei during the hottest period.  
 640 However, weak spots are noticed at the sunrise and sunset periods, a phenomenon  
 641 which has been named the alternating period of refrigeration (APR).
- 642 2. The APR issue can be alleviated by decreasing the heat transfer coefficient  $h_{bi}$  via  
 643 increasing the thickness of the air gap. When  $h_{bi}$  is  $0.5 \text{ W}/(\text{m}^2 \cdot \text{K})$ , the PT-AC  
 644 device's working time increases by about 60 minutes at sunrise and sunset

- 645 respectively compared with  $h_{bi}$  equals to  $2 W/(m^2 \cdot K)$ .  
 646 3. Also, APR can be further reduced by 2 hours by minimizing the heat transfer  
 647 coefficient between the bottom and the environment.  
 648 4. The new system has a more stable performance than the traditional PT-AC system.  
 649 The new system only needed an 11.5 kW·h sized thermal storage tank, which is 4  
 650 times smaller than the traditional PT-AC system. Moreover, it also correspondingly  
 651 occupied only half the required floor space.

## 652 ACKNOWLEDGMENTS

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 654 Universities (No. WK2090000021) and the Natural Science Foundation of Hefei, China  
 655 (Grant No. 2021048).

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## Highlights

- A new system combined AC and RSC is proposed to realize 24-h continuous cooling at smaller space and thermal storage.
- The steady-state model of this system is analyzed and compared with the traditional PT-AC.
- This system can meet the room heat load during most of the day except sunset.
- The performance can be improved significantly by reducing the convection and conduction heat loss.
- This system only needed a 4 times smaller thermal storage tank and half the floor space.

**Declaration of interests**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

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